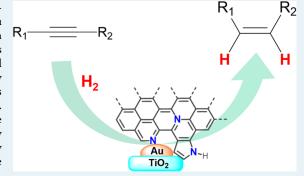
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# Accessing Frustrated Lewis Pair Chemistry through Robust Gold@N-Doped Carbon for Selective Hydrogenation of Alkynes

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Supporting Information

ABSTRACT: Pyrolysis of Au(OAc)<sub>3</sub> in the presence of 1,10-phenanthroline over TiO<sub>2</sub> furnishes a highly active and selective Au nanoparticle (NP) catalyst embedded in a nitrogen-doped carbon support, Au@N-doped carbon/TiO<sub>2</sub> catalyst. Parameters such as pyrolysis temperature, type of support, and nitrogen ligands as well as Au/ligand molar ratios were systematically investigated. Highly selective hydrogenation of numerous structurally diverse alkynes proceeded in moderate to excellent yield under mild conditions. The high selectivity toward the industrially important alkene substrates, functional group tolerance, and the high recyclability makes the catalytic system unique. Both high activity and selectivity are correlated with a frustrated Lewis pairs interface formed by the combination of gold and nitrogen atoms of N-doped carbon that,



according to density functional theory calculations, can serve as a basic site to promote the heterolytic activation of  $H_2$  under very mild conditions. This "fully heterogeneous" and recyclable gold catalyst makes the selective hydrogenation process environmentally and economically attractive.

KEYWORDS: gold, N-doped carbon, hydrogenation, alkyne, heterolytic cleavage, frustrated Lewis pairs

# **■ INTRODUCTION**

Alkenes have an extensive range of applications from intermediates in the chemical industry to their primary use as comonomers in the production of polymers. High-purity alkene feedstocks (alkyne free) for the polymer industry are obtained by a very fine-tuned catalytic hydrogenation process; the challenging selective hydrogenation of impurities (alkyne to alkene), while inhibiting the hydrogenation of the alkene to the alkane step and double-bond isomerization. The semihydrogenation of alkynes to alkenes is also known as a valuable synthetic strategy for drug design.<sup>2</sup> Typically, platinum group metal catalysts are very active for hydrogenations, but they usually suffer from the lack of selectivity to alkenes.3 Approaches to improve the chemoselectivity relied on addition of ligands, 5,6 usually nitrogen, phosphorus, sulfur, or addition of a second less-active metal.<sup>7,8</sup> In the context of hydrogenations, gold was less explored, 9,10 but is expected to be intrinsically selective for hydrogenation of triple bonds in alkyne-alkene mixtures, because of the preferential adsorption of only one of these components, the alkyne. 11 Nevertheless, gold-based

catalyst still suffer from the lack of activity, mainly due to limited capability to dissociate molecular hydrogen ( $H_2$ ), which usually is the rate-limiting step.<sup>3</sup> Cooperation between the coordinatively unsaturated Au atoms on the Au NPs and the acid—base pair site on  $Al_2O_3$ ,  $^{12,13}$  basic sites on hydroxyapatite  $^{14,15}$  and on ceria  $^{16,17}$  has been suggested as a strategy for the  $H_2$  dissociation to yield a  $H^+/H^-$  pair at the metal—support interface, which is then transferred to the organic moiety. Such heterolytic  $H_2$  splitting has been proposed to occur on pure oxides,  $^{18-20}$  on gold complexes,  $^{21-23}$  or due to a cooperation between gold and adsorbed basic ligands.  $^{24-30}$  We have recently systematically studied the activation of gold via the heterolytic dissociation of  $H_2$  based on the adsorption of nitrogen-containing bases on gold surfaces.  $^{24}$  The activation of  $H_2$  was proposed to occur at the metal—ligand interface forming a tight ion pair induced by a frustrated Lewis pair (FLP) like structure,  $^{31-35}$  which was able to promote the

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heterolytic activation of  $H_2$ , allowing a high activity and selectivity for the hydrogenation of alkynes into alkenes. In the proposed mechanism, identified by density functional theory (DFT), the  $H_2$  molecule splits forming a quaternary N center (amine protonation) and a hydride on the gold surface; both  $H^-$  and  $H^+$  were then transferred to the organic moiety in a *syn*-fashion controlled by electrostatic interactions.

Nitrogen-doped carbon materials affect the catalytic activity and selectivity of transition metals significantly, such as cobalt, 36,37 nickel, 38 palladium, 39,40 ruthenium, 41 and iron/ iron oxide-based catalysts. 42,43 The incorporation of nitrogen atoms in the carbon architecture combined with metal nanoparticles have enabled application in a wide range of catalytic reactions including reductions, oxidations, and H2 generation. 44,45 N-Doped carbon structures have also emerged as an important component of catalysts for hydrogenation reactions. 36,42,46,47 More interestingly, a heterolytic H<sub>2</sub> activation has been invoked to explain the hydrogenation reaction mechanism. 48-50 Although it is not explicit in the previous studies, it is likely that the metal-N-doped carbon interface can be understood as a FLP, with an active participation of the support basic nitrogen atoms in the H<sub>2</sub> activation. Based on our interest in this concept, we decided to explore the synthesis of gold nanoparticle catalysts embedded on N-doped carbon for studies in selective hydrogenations. The main advantage with respect to previous studies<sup>24</sup> is to avoid the addition of external ligands, in large excess, for the activation of gold surfaces via FLP, making the whole process environmentally and economically attractive.

#### RESULTS AND DISCUSSION

We commenced our study by preparing a series of gold catalysts inspired by the method developed by Beller's group for the preparation of Ni, Co, and Fe-catalysts.  $^{36,42,47,51,52}$  The gold catalysts were prepared by pyrolysis of the gold precursor at different temperatures in the range from 200 to 800 °C in the presence of 1,10-phenantroline (L1) and  $\text{TiO}_2$  support under  $\text{N}_2$  atmosphere (Figure S1). The thermal behavior TG-DTG of the Au-L1/TiO<sub>2</sub> material under  $\text{N}_2$  indicated that the pyrolysis proceeds in a multistage fashion (Figure S2). We studied the influence of the pyrolysis temperature on the catalytic activity of the various materials obtained for the benchmark hydrogenation of phenylacetylene 1a using molecular hydrogen (H<sub>2</sub>) (Table 1). The material pyrolyzed at 200 °C lead to 51% of

Table 1. Catalytic Activity in the Hydrogenation of Phenylacetylene of Au@N-Doped Carbon Catalysts Obtained from Au-L1/TiO<sub>2</sub> after Pyrolysis at Different Temperatures<sup>a</sup>

<sup>a</sup>Reaction conditions: 0.14 mmol 1a, 2 mol % of Au@N-doped catalyst, 2 mL of ethanol,  $100\,^{\circ}$ C, 6 bar H<sub>2</sub>, 20 h. Conversion and yield determined by GC using internal standard technique.

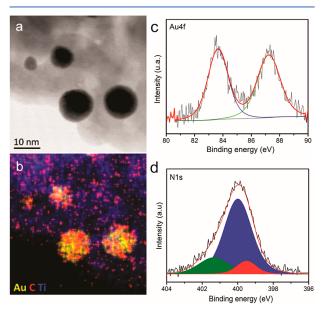
conversion of 1a (Table 1, entry 1). The best activity was obtained by performing the pyrolysis at 400 °C (Table 1, entry 2). On increasing the pyrolysis temperature to 600 and 800 °C, the activity of the resulting catalyst decreased significantly (Table 1, entries 3 and 4). We next studied the influence of the N-containing ligands on the stabilization and catalytic activity of the various materials obtained after pyrolysis at 400 °C (Table 2).

Table 2. Catalytic Activity in the Hydrogenation of Phenylacetylene of Au@N-Doped Carbon Catalysts Obtained with Different N-Containing Ligands, after Pyrolysis at 400  $^{\circ}\text{C}^a$ 

<sup>a</sup>Reaction conditions: 0.14 mmol of **1a**, 2 mol % of Au catalyst, 2 mL of ethanol, 100 °C, 6 bar of H<sub>2</sub>, 20 h. Conversion and yield determined by GC using internal standard technique; numbers in parentheses refer to isolated yield. <sup>b</sup>Catalyst not pyrolyzed.

Among the different N-containing ligands tested, 1,10phenanthroline (L1) was found to give the most-active system (Table 2, entry 1), resulting in a catalyst that exhibited superior reactivity in comparison with those obtained from other ligands such as 2,2'-bipyridine (L2), ethylenediamine (L5), diethylenetriamine (L6) (Table 2, entries 2, 5, and 6). The catalyst obtained using piperazine (L4) showed the lowest activity (Table 2, entry 3). Moreover, the model reaction does not occur to any extent in the presence of the material not submitted to pyrolysis (Table 2, entry 7). Notably, the catalyst prepared without addition of any ligand (Au/TiO<sub>2</sub>) showed significant low catalytic activity (Table 2, entry 8), and no conversion was observed with a material obtained via pyrolysis of the support with 1,10-phenantroline (L1/TiO<sub>2</sub>) but without the gold precursor (Table 2, entry 9). We further investigated the potential effect of supports (C, CeO<sub>2</sub>, MgO, Fe<sub>3</sub>O<sub>4</sub>, SiO<sub>2</sub>, and TiO<sub>2</sub>) in the catalytic activity (Table S1). The catalysts based on carbon, cerium oxide, iron oxide, and magnesium oxide showed low conversion ( $\leq 10\%$ ). The catalyst supported on silica reaches 71% of conversion, but the fully hydrogenated product 3a was formed. Titanium dioxide proved to be the best support under the studied conditions. The gold precursor

influence of the catalytic activity was also evaluated (Table S2). The catalyst prepared using gold acetate showed the best result, full conversion of 1a, and a slight decrease in catalytic activity was noticed when using hydrogen tetrachloroaurate(III) (68% of conversion) or potassium dicyanoaurate(I) (90% of conversion). An increase in the Au/L1 molar ratio from 1:2 to 1:5 or 1:10 led to complete loss of catalytic activity (Table S3). After a further survey of common reaction parameters (solvent, reaction temperature, molecular hydrogen pressure; for more details, see Tables S4, S5 and S6 at the Supporting Information), the best reaction conditions were ethanol as solvent, 6 bar of H<sub>2</sub> at 100 °C. The most active catalytic material obtained by pyrolysis at 400 °C was characterized in detail. The active catalyst contains 1.1 wt % Au, 0.7 wt % C and 0.2 wt % N, as determined by elemental analysis and FAAS. Images by scanning transmission electron microscopy (STEM) of the material pyrolyzed with the L1 ligand revealed formation of Au NPs with a mean diameter of 4.5 nm, in addition, a few larger particles of 10 nm were observed occasionally (Figure S3a-c). In complete contrast, the catalyst prepared without the presence of the ligand, a significant increase in the gold NPs size was observed, with a mean diameter about 17 nm (Figure S3d-f). UV-vis diffuse reflectance spectra were recorded for both solids (with and without L1), showing a typical gold SPR band (Figure S4). The X-ray diffraction (XRD) pattern corresponding to Bragg diffractions of Au (200) at 44°, Au (220) at 65°, or Au (311) at 78°, confirmed the metal reduction and anatase as the predominant phase, without significant phase conversion after thermal treatment (Figure S5). EDX spectrum imaging (elemental mapping) of the Au-L1/TiO<sub>2</sub> material after pyrolysis at 400 °C provided a clear evidence for the presence of carbon deposited on the surface of the Au NPs (Figure 1). No conclusive information on the location of nitrogen in the sample could be obtained because of



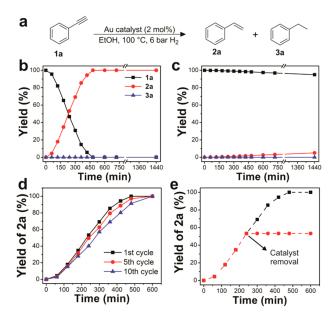
**Figure 1.** (a) Bright-field STEM image of a representative area of the Au@N-doped carbon/TiO $_2$  catalyst (Au-L1/TiO $_2$  material after pyrolysis at 400 °C) and (b) corresponding EDX elemental maps. Carbons appear as the red spots deposited mostly on the yellow gold particles. (c) Au 4f XPS spectrum and (d) N 1s XPS spectrum for the Au@N-doped carbon/TiO $_2$  catalyst.

the overlap of the majoritarian Ti signal at 0.452 keV with the N signal at 0.392 keV (Figure S6).

The type of N-doping was investigated in more detail by Xray photoelectron spectroscopy (XPS). The XPS survey spectrum of catalytic material obtained by pyrolysis at 400 °C revealed that the samples surface contains Au, C, Ti, N, and O. The Au 4f spectrum exhibit two peaks centered at binding energy 87.0 and 83.3 eV, which correspond to the Au<sup>0</sup> oxidation state<sup>53,54</sup> (Figure 1c). Valuable information was obtained by analysis of the binding energy peak of the N 1s region (Figure 1d and Figure S7-S9). The N 1s spectrum of the most active Au@N-doped carbon catalyst (pyrolysis at 400 °C) was fitted with three components located at binding energies of 399.5, 400, and 401.3 eV (Figure 1d). The peak at 401.3 eV can be attributed to graphitic nitrogen, while the peak at 399.5 eV can be attributed to the pyridinic nitrogen species. 44,55,56 However, the peak at 400 eV is more difficult to attribute, as it can be both a result of Au-N interaction (see results for Au-L1/TiO<sub>2</sub> (before pyrolysis), Figure S9) or due to pyrrolic nitrogen species, very often present in N-doped carbon systems,<sup>46</sup> and also present in the XPS N 1s spectrum of the sample L1/TiO<sub>2</sub> (without gold) (Figure S7). This component at ca. 400 eV was found in all catalysts prepared by pyrolysis with other ligands (L2-L6) at 400 °C (Figure S8) and for Au/ L1-TiO<sub>2</sub> at other pyrolysis temperatures (Figure S9). The asprepared catalyst precursor Au-L1/TiO<sub>2</sub> (before pyrolysis) displays two nitrogen species at 399.3 and 399.8 eV (Figure S9), which are tentatively attributed to pyridinic nitrogen atoms of free ligand and of the ligand coordinated and/or adsorbed on gold (Au-N), respectively. The 1,10-phenanthroline ligand adsorbed on TiO2 (L1/TiO2 without gold) displays only one nitrogen species at 399.4 eV (Figure S7), typically of a pyridinic nitrogen atom (free ligand).

The kinetic study shown in Figure 2b indicates full conversion of 1a to 2a in about 8 h and suppression of further hydrogenation of 2a to 3a, even at long reaction times. This high selectivity for the alkene 2a is an intrinsic property of our catalyst and it was not observed for the well-known Pd Lindlar catalyst (Pd/CaCO<sub>3</sub> + Pb(OCOCH<sub>3</sub>)<sub>2</sub> + quinoline), which produces 3a at high conversions (Figure S10). It is worthwhile to note that a sixty-fold reaction rate enhancement was observed when comparing the catalytic activity of similar Au catalysts prepared with L1 (Figure 2b) (reaction rate = 0.273 mmol g<sub>cat</sub> -1 h<sup>-1</sup>) or without any ligand (Figure 2c) (reaction rate = 0.00472 mmol  $g_{cat}^{-1}$  h<sup>-1</sup>). In order to further examine the stability as well as recyclability of the "fully heterogeneous" catalytic material, the hydrogenation of 1a was repeated up to 10 times using the same catalyst portion without any further treatment or ligand addition. As depicted in Figure 2d, the desired product styrene 2a was obtained in a 99% yield even after ten runs and no significant loss of activity was observed (see also Figure S11). A hot filtration test (Figure 2e) revealed that the obtained activity is not related to any leaching of the catalytically active metal (no remaining activity in the supernatant). ICP AES analysis of the recycling experiments indicated no undesired leaching processes of gold occurred during the course of the catalytic transformation. Furthermore, no aggregation of Au NPs was observed by STEM of the recycled catalyst after the 10th recycle (Figure S12).

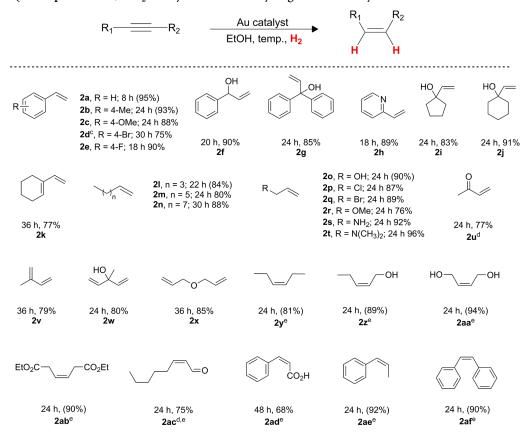
Because Au@N-doped carbon/TiO<sub>2</sub> catalyst (Au-L1/TiO<sub>2</sub> pyrolyzed at 400 °C) displayed the best activity for the production of styrene, it was explored in the scope study under the optimized conditions. A variety of terminal and internal



**Figure 2.** (a) Time course of hydrogenation of phenylacetylene **1a** catalyzed by (b) Au@N-doped carbon/TiO<sub>2</sub> catalyst and (c) Au/TiO<sub>2</sub> catalyst; (d) recycling experiments and (e) hot filtration test to determine homogeneous catalysis contribution in hydrogenation of **1a**. Reaction conditions: 0.14 mmol of **1a**, 2 mol % of Au, 2 mL of ethanol, 100 °C, 6 bar of H<sub>2</sub>.

alkynes was readily hydrogenated to the desired alkene and cisalkene with moderate to excellent yield (Scheme 1) and, notably, different from what occur with other transition metals, without any over-reduction to alkane. Moreover, both electrondeficient substituents, such as esters (2ab) and carboxylic acids (2ad) moieties, and electron-rich groups, for example amino (2s and 2t) and methoxy (2c and 2r), were tolerated well. The developed catalyst was even able to reduce only the alkyne unit in molecules with alkene moieties (2k, 2v, 2w, and 2x), without any detectable concurrent reduction of the alkene moieties both in the parent and product molecules. The results depicted in Scheme 1 confirmed that a broad range of sensitive and reducible functional groups, including halide (2d, 2e, 2p, and 2q), ketones (2u), and aldehydes (2ac), were tolerated in the alkyne hydrogenation process. With an increase in H2 pressure (10 bar H<sub>2</sub>), (Z)-alkenes were mostly formed from internal alkynes (2y-2af). The catalyst system was also applicable for scaled-up conditions, where 5 mmol of 1a (0.51 g) was successfully converted into the alkene 2a (0.49 g, 94%). Considering full conversion, the turnover number (TON) of 1700 was reached, with a TOF of 70 mol  $mol^{-1} h^{-1}$ . This TOF value is an order of magnitude higher than the values reported for heterogeneous gold-based catalysts using molecular hydrogen as hydride source and without the use of ligands. Furthermore, this TOF is also high when taking into account values for systems using other sources of hydride and ligands to boost the catalytic activity (Table S7).

Scheme 1. Au@N-Doped Carbon/TiO<sub>2</sub> Catalyst for the Semihydrogenation of Alkynes to Alkenes<sup>a, b</sup>



<sup>&</sup>quot;Reaction conditions: 0.14 mmol of alkyne, 2 mol % of Au catalyst, 2 mL of ethanol at 100 °C, 6 bar of H<sub>2</sub>. <sup>b</sup>GC yields are shown; values in parentheses refer to isolated yields. Selectivity was >99%. <sup>c</sup>8 bar of H<sub>2</sub>. <sup>d</sup>80 °C. <sup>e</sup>10 bar of H<sub>2</sub>.

To further check the chemoselectivity of the developed catalyst, we performed experiments using 1a as substrate in the presence of molecules functionalized with other sensitive groups (Scheme 2). Total chemoselectivity was observed for

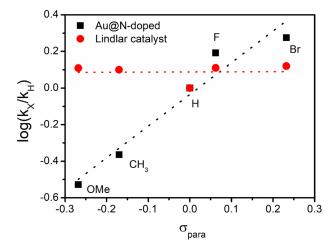
Scheme 2. Selective Hydrogenation of 1a in the Presence of Molecules with Other Reducible Functional Groups by Au@ N-Doped Carbon/TiO<sub>2</sub> Catalyst<sup>a</sup>

<sup>a</sup>Reaction conditions: 0.14 mmol 1a, 0.14 mmol of sensitive molecule, 2 mol % of Au catalyst, 2 mL of ethanol, 24 h, 100 °C, 6 bar H<sub>2</sub>. Conversion was determined by GC using internal standard technique.

the reduction of the model alkyne in the presence of potentially reducible groups, such as nitro, aldehydes, epoxides, ketones, nitriles, esters, heteroaromatic *N*-oxides, and amide, because not even traces of conversion of these functional groups were detected. In the absence of the alkyne, some of those functional groups such as epoxides, nitro, aldehydes, heteroaromatic *N*-oxides, and sulfoxides can be efficiently reduced as well (Table S8).

On the basis of the experimental results and previous work, we believe that pyridinic, graphitic, and pyrrolic N atoms play a pivotal role in boosting the catalytic activity of our gold-based catalyst. The reactivity pattern displayed by the Au@N-doped carbon catalyst, prepared via pyrolysis of Au-L1/TiO2, allows us to postulate that H2 activation may proceed by a heterolytic pathway, due to the interaction of Au NPs and the nitrogen atoms of the N-doped carbon around the metallic nanoparticles, following the concept of frustrated Lewis pair interface suggested before for Au NPs and externally added N-containing ligands.<sup>24</sup> This type of H<sub>2</sub> activation at N-doped carbon supports was previously described for Pd, 48 boronnitrogen codoped graphene,<sup>57</sup> and Co catalyst.<sup>49</sup> introduction of N atoms might affect the properties of the supported catalyst, such as tunable acid-base character at the support surface, which could cause a better interaction of metal-support-reactant, as well as charge transfer phenomena at the metal-support junction.44

In order to gain more insight into the mechanism of the reaction, we conducted a Hammett correlation study using the developed catalyst and Lindlar catalyst to verify the influence of various para substituents on aromatic alkynes. The Hammett plot for the reaction catalyzed by Au@N-doped carbon catalyst reveals that the reaction is sensitive to the substituent (Figure 3). The reaction rate was enhanced in the presence of electron-withdrawing groups, and the positive value of  $\rho$  ( $\rho$  = +1.73;  $R^2$  = 0.93) highlights the buildup of negative charge during the catalytic cycle. The value of  $\rho$  with Lindlar catalysts was close to

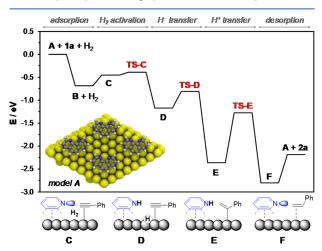


**Figure 3.** Hammett plot for the hydrogenation of various parasubstituted alkynes catalyzed by Au@N-doped carbon/TiO $_2$  and Lindlar catalyst.

0, which indicates a lack of substituent effect in the hydrogenation reaction and that no charge is built or lost during the catalytic cycle. Those results give support to a heterolytic  $H_2$  dissociation mechanism for the Au@N-doped carbon catalyst, in contrast to the homolytic  $H_2$  activation mechanism for Lindlar catalyst. Moreover, theoretical calculation and experimental results have demonstrated that nitrogen doping structures could also enhance the stability of Au catalyst against sintering, preserving the catalytic activity,  $^{54,58,59}$  which explains the high recyclability and lack of particle aggregation.

On the basis of the results described above, we propose that the nitrogen atoms doped on carbon have a major role in the heterolytic activation of H<sub>2</sub> via frustrated Lewis pairs. To support such hypothesis, we present a computational study of the hydrogenation mechanism of alkyne 1a. Following previous experiments (Table 2, entry 1), we model a Au(111) surface functionalized with phenanthroline L1. Taking into account the high coverage situation of the experiments, the  $\pi$ -system of L1 may adsorb in two main configurations: (i) parallel (flat) to the surface, model A, or (ii) perpendicular to it, model A2. Model A contains one L1 in the supercell, while model A2 can fit up to three (Figure S13). Both situations present the same adsorption energy ( $E_{ads}$ ) per ligand, (-0.74 and -0.75 eV, respectively, Table S9), with the shortest Au···N distances of ca. 3.3 and 3.5 Å, respectively. At high coverage situations, the packing predicted in model A2 would be expected, and in operando conditions, ligands would be replaced by reactant molecules via 0.75 eV. Such a continuous release of ligand compromises the robustness of the catalyst. After pyrolysis treatment, however, aromatic rings agglomerate to form extended graphene-like sheets. From literature we know that the  $E_{\rm ads}$  of benzene on Au(111) is 0.63 eV (experiment)<sup>60</sup> and 0.48 eV (theory);<sup>61</sup> in other words, ca. 0.08 eV per sp $^2$  atom. The  $E_{\rm ads}$  of L1 (14 sp $^2$ atoms) on Au(111) in model A is 0.74 or 0.05 eV/sp<sup>2</sup>, somehow smaller than that of benzene. The hypothetical merging of two L1 ligands (28 sp<sup>2</sup> atoms) would render a new species with a significantly larger  $E_{\rm ads}$  of ~1.4 eV. In contrast to free ligand conditions, where ligands can be easily displaced, extended graphene-like sheets anchor to the surface, thus creating a stable and robust system while maintaining the nature of the catalytic active site.

Herein we use model A (Figure 4 inset) to properly mimic the N-doped (pyridinic) graphene-like sheets experimentally



**Figure 4.** Computed reaction energy profile for the hydrogenation of 1a on L1-functionalized Au(111) surface (Au = yellow, N = blue, C = gray, H = white).

observed after pyrolysis. The proposed reaction mechanism is shown in Figure 4. First, the alkyne 1a interacts with the surface A with an energy of -0.69 eV (B). Although subsequent  $H_2$ adsorption (C) is slightly endothermic by 0.23 eV, the Nassisted heterolytic H<sub>2</sub> activation (TS-C) is essentially barrierless, with a relative energy barrier of 0.07 eV above C (0.30 eV above B). Moreover, the formation of D is significantly exothermic by 0.71 eV. These results are in sharp contrast with the  $H_2$  dissociation on pristine Au(111), where the energy barrier is 1.45 eV and the reaction energy is endothermic by 0.69 eV.<sup>24</sup> The absence of a direct interaction between the lone pair of the nitrogen and the gold surface (Au...N distances of ca. 3.3 Å) creates a unique interface that promotes the heterolytic cleavage. In that sense, we can relate this behavior to gold-based FLP chemistry. 62 Then, the hydride from the surface D eventually transfers to the alkyne (TS-D) with a barrier of 0.36 eV and forms the alkenyl intermediate E. Final proton transfer from nitrogen to carbon has a barrier of 1.09 eV (TS-E) and produces intermediate F, from which the product 2a quickly desorbs (0.62 eV) and regenerates the initial species A. Overall, the present mechanism is in line with experiments and ilustrates the major role of nitrogen atoms during the H<sub>2</sub> activation process.

#### CONCLUSIONS

We have prepared, for the first time, a N-doped carbon supported gold-based catalyst that exhibited excellent activity and selectivity for the hydrogenation of alkynes to alkenes, in a broad scope of substrates, at mild reaction condition. The intriguing structure of the novel gold heterogeneous catalyst, which could be understood as frustrated Lewis pairs interfaces according to computational studies, enables the heterolytic activation of molecular hydrogen, boosting gold catalytic activity while avoiding addition of external ligands to improve activity and selectivity. The graphenization of the ligand ensures that it is present on the surface and not removed by the solvent or the reactants, which explains the robustness of the material under reaction conditions. We demonstrated that the heterolytic dissociation of  $H_2$  can occur in a fully heterogeneous

catalyst, which will be economically and environmentally attractive. The Au@N-doped carbon catalyst tolerates other reducible functional groups, including C–C double bonds, nitro, aldehydes, epoxides, ketones, nitriles, esters, heteroaromatic N-oxides, and amides, and they can be recycled without loss of activity. The surface-FLP concept is in its infancy when compared to main group-FLP<sup>32,63</sup> and transition metal-based FLP,<sup>64</sup> but has shown many interesting features. The expansion of this concept for a broad range of applications in the field of heterogeneous catalysis is encouraged. New reactivity patterns, not limited to activation of H<sub>2</sub>, will be soon explored.

#### EXPERIMENTAL SECTION

**Procedure for Preparation of Au-L/Support.** Typically,  $Au(OAc)_3$  (19 mg, 0.05 mmol) and amine ligand (18 mg, 0.1 mmol) (molar ratio Au:L=1:2) were stirred in 20 mL of ethanol for approximately 5 min at 60 °C. The support was then added and the mixture was stirred for more 20 min. Afterward, the solvent was dried by rotary evaporation. The asobtained solid was ground to a fine powder and then pyrolyzed under nitrogen atmosphere in the desired temperature in an oven at a rate of 10 °C per minute and held at temperature for 2 h.

General Procedure for Hydrogenation of Alkynes. Unless otherwise stated, a typical procedure for the semihydrogenation of alkynes is as follows: alkyne (0.14 mmol), Au catalyst (2 mol % Au), and 2 mL of solvent were placed in a modified Fischer-Porter 100 mL glass reactor. The reactor was purged five times with H2, leaving the vessel at 6 bar. The resulting mixture was vigorously stirred, and the temperature was maintained with an oil bath. After the desired time, the catalyst was removed by centrifugation, and the products were analyzed by GC with an internal standard to determine the conversion of alkyne and the selectivity for alkene. To determine the isolated yield of the obtained products, after the reaction was complete, the solvent was evaporated, and the crude reaction mixture was purified by column chromatography on silica gel to afford corresponding alkenes. <sup>1</sup>H confirmed the purity of the isolated products.

**Computational Details.** All calculations were performed at Density Functional Theory (DFT) level using the Vienna Abinitio Simulation Package (VASP).65,66 We use the PBE functional<sup>67</sup> supplemented with Grimme's D2 dispersion scheme<sup>68</sup> and refined parameters for transition metals.<sup>61</sup> Core electrons were described by projector augmented wave (PAW) pseudopotentials<sup>69</sup> and valence electrons by a kinetic energy cutoff of 450 eV. The Au(111) surface was modeled by a  $(4 \times$ 4) supercell with four-layer thick slabs, where the two upper layers were relaxed and the two bottom ones were fixed to mimic the bulk. The Brillouin zone was sampled by a  $3 \times 3 \times 1$ k-points mesh, generated through the Monkhorst-Pack method. To avoid spurious interactions between the periodic images, a vacuum region between the slabs of 15 Å and dipole correction along z were included.<sup>71</sup> Transition states were located with the climbing image nudged elastic band (CI-NEB) method.<sup>72</sup> The assessment of the minima and transition states was performed by diagonalizing the numerical Hessian matrix obtained by ±0.015 Å displacements. Metal and ligand atoms were fixed during frequency calculations. All inputs and final structures can be found in the ioChem-BD repository. 73,7

#### ASSOCIATED CONTENT

# Supporting Information

Experimental details, additional experimental results, characterization of the catalyst (XRD, TEM, UV-vis), and L1/Au adsorption energies (PDF)

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#### Notes

The authors declare no competing financial interest.

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